Addressing Internal "Shuttle" Effect: Electrolyte Design and Cathode Morphology Evolution in Li-S Batteries

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June 9th, 2016

Project ID #: ES283

Overview

Timeline

- Start date: October 1, 2014
- End date: September 30, 2017
- Percent complete: 50%

Budget

- Total funding: \$990,000
 - DOE share: \$990,000
 - Contractor share: Personnel
- Funding received
 - FY15: \$285,345
 - FY 16: \$325,189

Barriers

- Barriers/targets addressed
 - Loss of available capacity
 - Materials evolution during cycling
 - Lifetime of the cell

Partners

- Interactions/ collaborations
- Partha Mukherjee (TAMU Co-PI)
- Vilas Pol (Purdue Univ., Co-PI)
 - Project lead: TAMU

Relevance/Objectives

- Objective: Overcome Li-metal anode deterioration issues via protective passivation layers and minimizing polysulfide shuttle with advanced cathode structure design.
- FY 2016 goals: Understand Li₂S deposition reactions; influence of cathode mesostructure on strain accommodation; and SEI nucleation in presence of polysulfides with atomistic and mesoscopic modeling and coir cell testing.

Addressing targets and barriers:

 Controlled cathode mesoporous structures synthesized with a novel sonochemical method and new electrolyte formulations based on mesoscale and atomistic modeling efforts.

Impact:

 Alternative electrolyte chemistries and improved cathode architectures to deliver Li/S cells operating for 500 cycles at efficiency greater than 80%.

Relevance/Milestones

- a) Synthesis of C/S hybrid cathode materials and advanced characterization. (Dec. 14) Completed
- b) Determine structure and reactivity of PS/Li interface. (Mar. 15).
 Completed.
- c) Identification of reactions at the C/S cathode. (June 15).
 Completed.
- d) Analysis of cathode microstructure with mesoscopic model and experimental characterization. (Sept.15) Completed (Go/No-Go)
- e) Coin cell testing of C/S electrodes. (Dec.15) Completed
- f) Electrochemical and transport analysis of deposition and diffusion rates in composite cathodes- (Mar.16) Completed
- g) Influence of mesostructure on strain accommodation (June 16)
 (Ongoing)
- h) Reaction mechanisms and SEI formation at the Li anode in presence of PS species (Sep. 16) (Ongoing) (Go/No-Go)

Approach/Strategy

Overall <u>Technical Approach/Strategy</u>:

- A mesoscale model of electrode mesoporous structures based on stochastic reconstruction allows virtual screening of cathode microstructural features and effects on electronic/ionic conductivity and morphological evolution.
- Interfacial reactions at the anode due to the presence of polysulfide species will be characterized with ab initio methods.
- Data and detailed structural and energetic information from atomistic-level studies used in mesoscopic-level analysis of cathode interfacial reactions.
- Novel sonochemical fabrication method for controlled cathode mesoporous structures and new electrolyte formulations based on mesoscale and atomistic modeling efforts.
- Progress towards FY15 and FY16 milestones and Go/No Go decisions: New understanding of interfacial anode chemistry and deposition reactions at the cathode. Analysis and test of 5 materials for PS retention at the cathode.

Technical Accomplishments: Barriers Addressed

Complexity of Li metal reactivity

 Characterized PS decomposition at the Li metal anode and formation of a Li₂S film

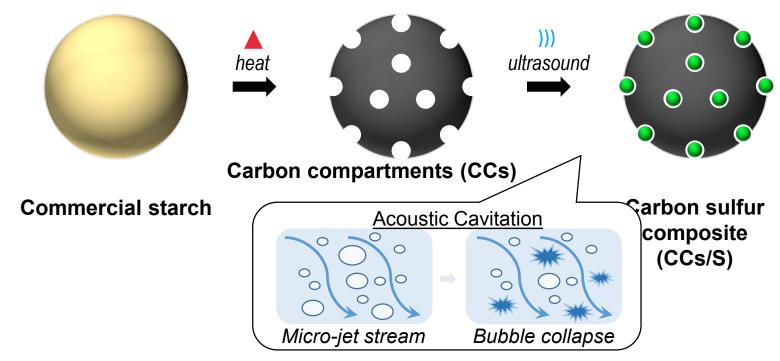
Control of cathode microstructure

 Novel sonochemical process allows for low-cost and simple process for fabrication of effective C-S cathodes.
 Mesoscopic modeling reveals effects of microstructure on macroscopic properties

PS retention at cathode

Identified and tested specific materials to retain soluble PS species at the cathode

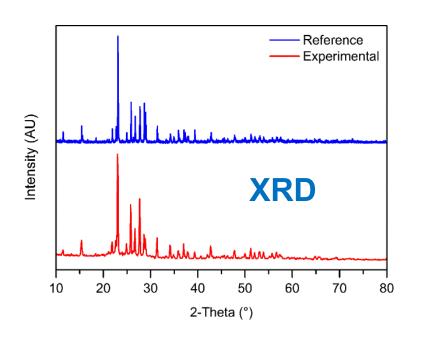
Technical Accomplishments Carbon compartments/S composites

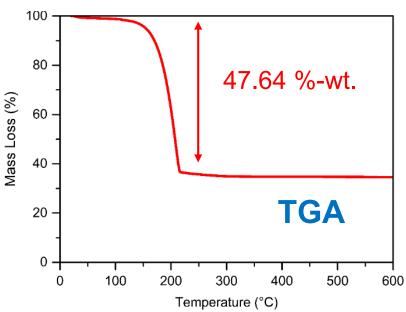


- Pyrolysis of starch produces a porous carbon substrate.
- Sonochemistry allows high T (5000 K), high P (1000 atm), rapid thermal rates (100K/s), and stream speeds (400 km/h) via acoustic cavitation.
- Sonochemical reduction of Na₂S₂O₃ to S in presence of dil HCl_(aq)

Milestone Q1/Y1: Lab scale C/S composite synthesized and characterized

Technical Accomplishments CC/S composites: characterization



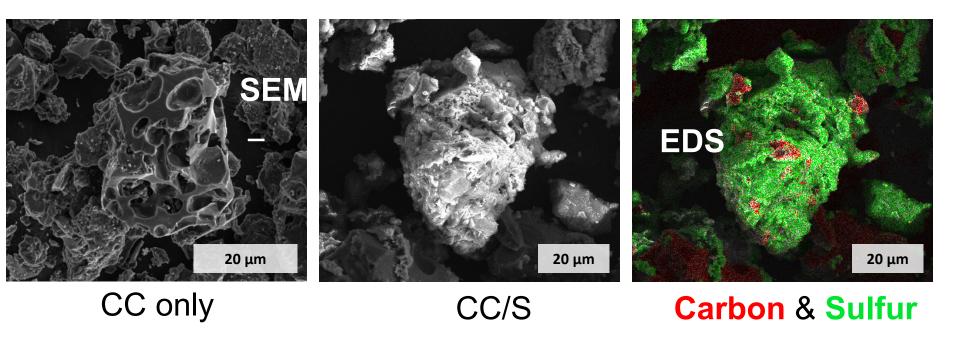


- Orthorhombic α-sulfur formed in the composite via sonochemical synthesis (from XRD analysis)
- 47.64 %-wt. sulfur loaded into the CC/S composite (from TGA analysis)



Lab scale C/S composite synthesized and

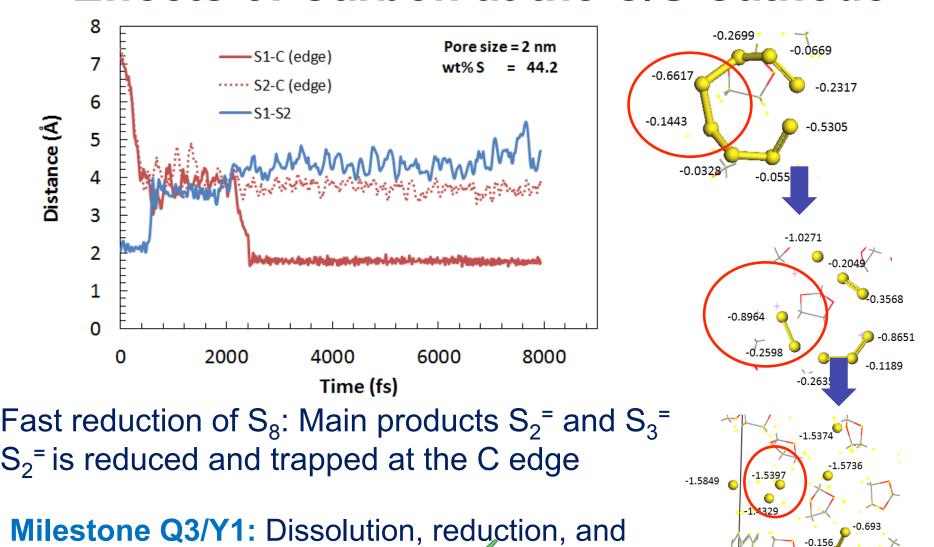
Technical Accomplishments CC/S composites: SEM & mapping



- Pyrolysis of commercial starch produces a bimodal-porous carbon with large micro-compartments and small pores
- Sonochemical procedure creates a thin layer of sulfur coating surface and inhabiting pores

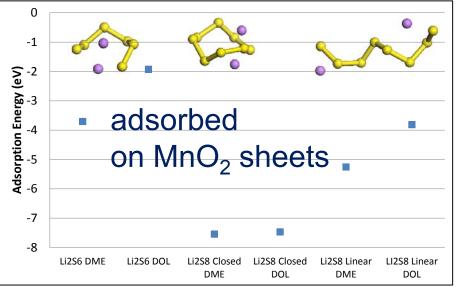
Milestone Q1/Y1: Lab scale C/S composite synthesized and characterized

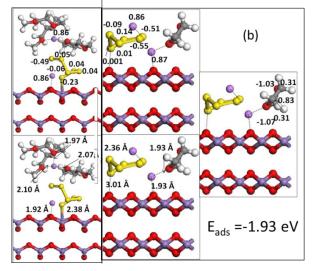
Technical Accomplishments: Effects of Carbon at the C/S Cathode



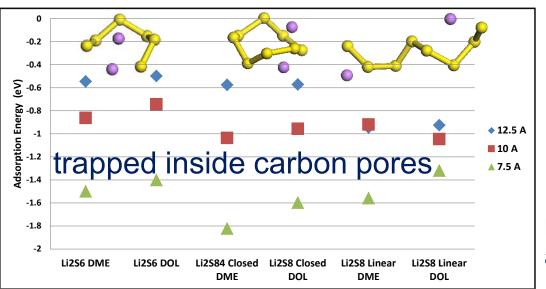
lithiation of S at the C-S cathode

Technical Accomplishments: Soluble PS Retention at the Cathode Surface PS can





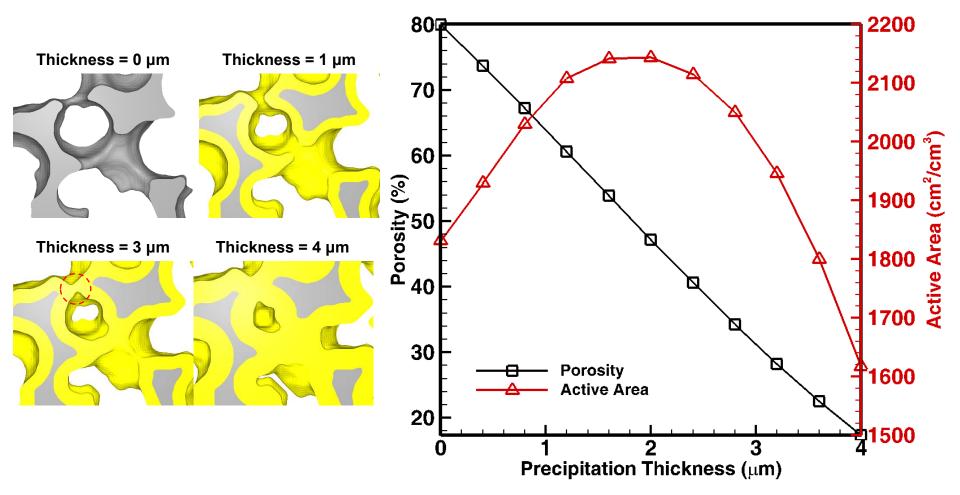
form strong covalent bonds but no dissociation was found on the MnO₂ (001) plane in contrast to Fe_2O_3 surfaces



PS retention mechanisms have been identified

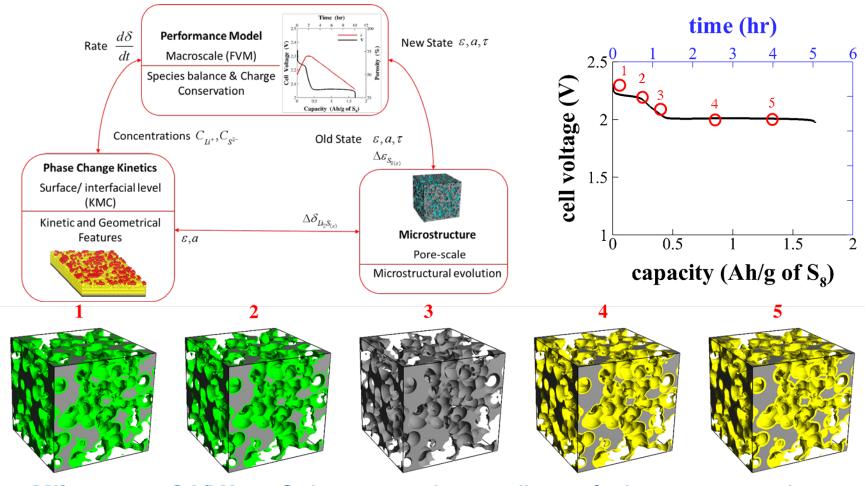
Milestone Q3/Y1: Dissolution, reduction, and lithiation of S at C-S cathode

Technical Accomplishments: Microstructure variation due to deposition



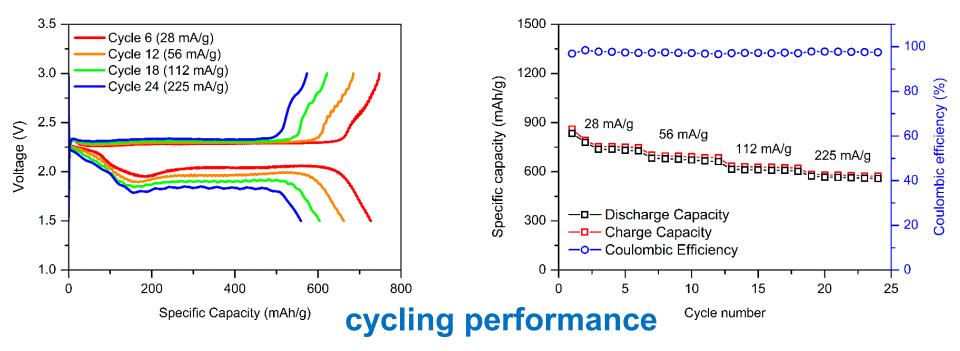
Milestone Q4/Y1: Elucidate cathode morphology evolution and microstructure transport interaction

Technical Accomplishments: Multiscale Modeling of Li-S Battery



Milestone Q2/Y2: Gain an understanding of the mesoscopic reactions using electrochemical and transport modeling

Technical Accomplishments CC/S composites: rate performance



- 750mAh/g capacity at 28 mA/g specific current.
- Electrolyte: DOL (50 %-vol.),1,1,2,2-tetrafluoroethyl-2,2,3,3-tetrafluoropropyl ether (50 %-vol.), Li TFSI salt (1.0 M conc.)

Milestone Q1/Y2: Coin cell testing of C/S electrodes



Technical Accomplishments: Reactivity of Soluble PS at the Li Metal Anode

Long-chain Li₂S₈ polysulfide extremely reactive with lithium

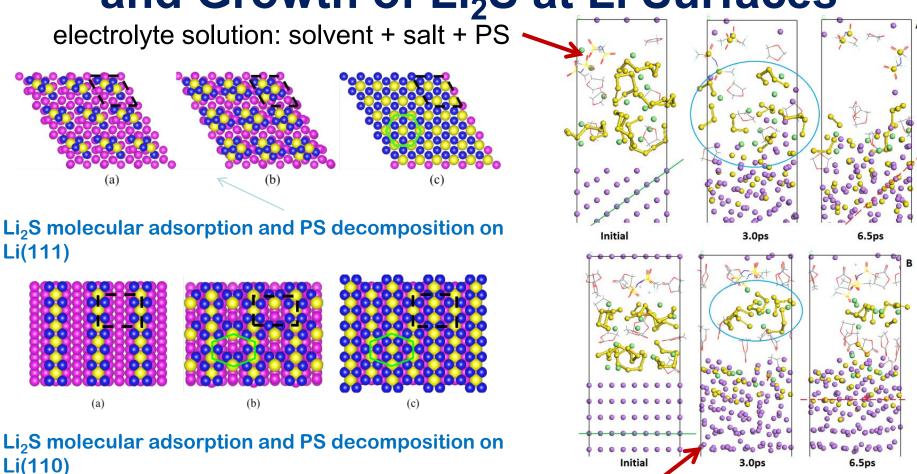
	Gas-Phase		EC Solvent		DOL Solvent	
Possible reactions	∆E (0K)	∆ G(298K)	∆E (0K)	∆ G(298K)	∆E (0K)	∆ G(298K)
Li ₂ S ₈ +2Li→Li ₂ S+Li ₂ S ₇	-3.56	-3.43	-5.53	-5.39	-5.18	-4.85
Li ₂ S ₈ +2Li→Li ₂ S ₂ +Li ₂ S ₆	-5.63	-5.38	-6.02	-5.92	-5.64	-5.51
Li_2S_8 +2 Li_2S_3 + Li_2S_5	-5.32	-5.17	-6.19	-6.09	-5.78	-5.65
Li ₂ S ₈ +2Li→2Li ₂ S ₄	-6.95	-6.69	-6.28	-6.14	-6.15	-5.98

All reactions exothermic and $\Delta G < 0$ (spontaneous). Energies in eV

Milestone Q2/Y1: Nucleation and growth of PS deposits at Li metal surface

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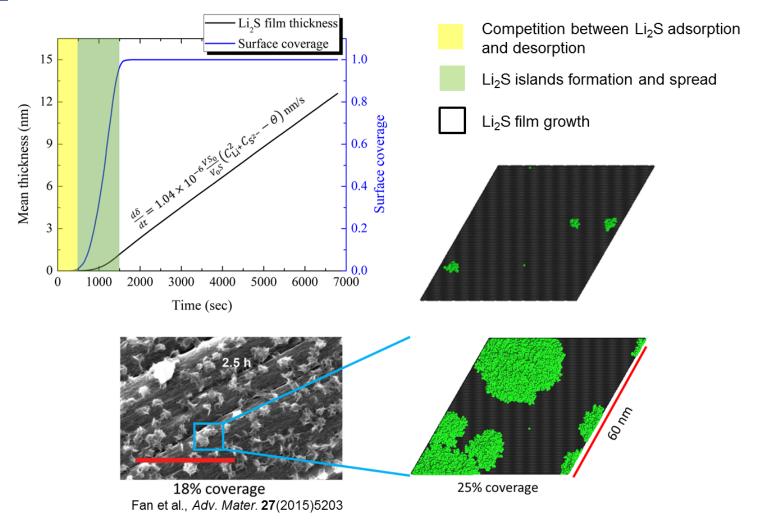
Technical Accomplishments: Nucleation and Growth of Li₂S at Li Surfaces



PS (yellow) extremely reactive; decomposes before salt or solvent

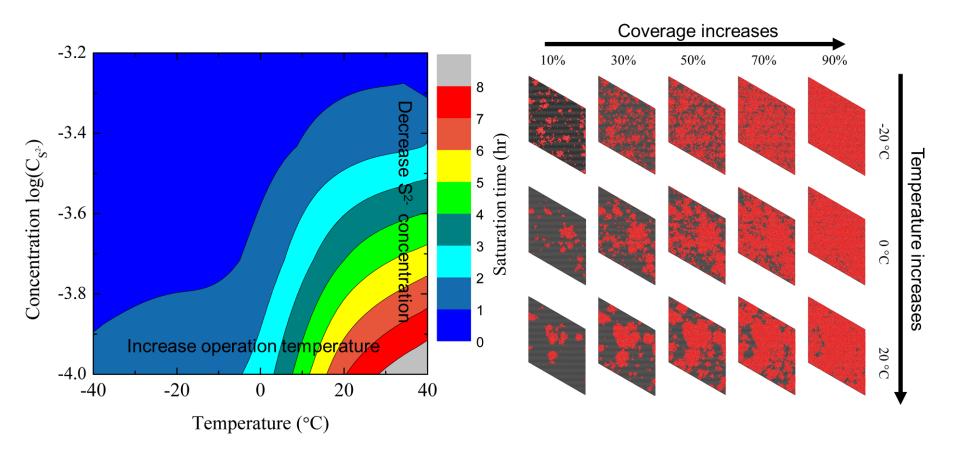
Milestone Q2/Y1:Thermodynamics and kinetics of nucleation and growth of PS deposits at the Li metal surface

Technical Accomplishments: Li₂S Film growth: Mesoscale modeling



Milestone Q2/Y1: Characterization of thermodynamics of nucleation and growth of PS deposits on the Li surface

Technical Accomplishments: How to defer the surface passivation



Milestone Q2/Y1: Characterization of thermodynamics of nucleation and growth of PS deposits on the Li surface

Responses to Previous Years Reviewers' Comments

This project started FY15; it was not evaluated last year

Collaboration and Coordination with Other Institutions

- Purdue University: This project is a collaboration between Texas A&M University (Balbuena, Mukherjee) and Purdue University (Pol). The groups communicate via teleconference and site visits.
- Pacific Northwest National Laboratory (PNNL): The TAMU team interacts with the group of Dr. Jason Zhang regarding analysis of strategies to mitigate extreme Li metal reactivity. We are currently investigating the reasons for the apparent mitigation effects caused by high salt concentrations as a function of the nature of the salt.
- Argonne National Laboratory (ANL): Dr. Vilas Pol (Purdue) collaborates with the group of Dr. Jeffrey Elam and Dr. Anil Mane at ANL in the applications of ALD coatings for polysulfide capture at the cathode.

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Remaining Challenges and Barriers

- Characterize SEI reactions at the Li metal anode and effects of higher salt concentration on such reactions.
- Evaluate influence of mesostructure on strain accommodation in the cathode.
- Identify reasons for failures and successes of specific electrolyte compositions and impact on Li anode behavior.
- Estimate the influence of cathode microstructure and electrolyte properties on cathode performance.
- Scale up of cathode composites.

Proposed Future Work

Rest of FY16:

- effects of deposition induced stress in cathode structure
- mechanisms of SEI reactions at anode as functions of electrolyte composition
- reasons for electrolyte failure and success

• FY17:

- influence of cathode structure and electrolyte properties on cell performance
- develop stable electrolytes
- produce 3-5gr of C/S composite and achieve capacity800 mAh/g during at least 400 cycles

Summary Slide

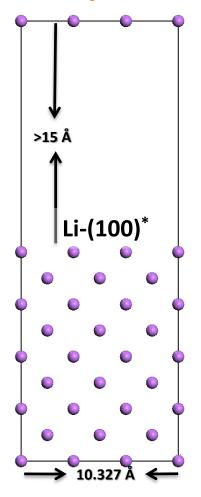
- Relevance: Overcome Li-metal anode deterioration issues via protective passivation layers and minimizing polysulfide shuttle with advanced cathode structure design.
- Approach: Synthesis, characterization, and testing of a C/S composite cathode guided by multiscale modeling (atomistic and mesoscopic) focusing on electrolyte composition and cathode morphology effects on cell performance.
- Technical Accomplishments: Development of low-cost synthesis and characterization of a C/S composite cathode with promising performance; identification of effects of carbon on sulfur reductions; effects of microstructure variation due to deposition; elucidation of reactions of the polysulfides on the Li metal anode.
- Collaborations: Purdue University (Co-PI); evaluation of additives and salts (with PNNL); cathode coatings (with ANL).
- Future Work: Development of stable electrolytes; scale up cells and achieve target capacity; model effects of cathode microstructure on cell performance.

Technical Back-Up Slides



Methodology

DFT optimization: Anode Model and Electrolyte Species



Anode Model

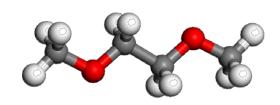
EC Ethylene carbonate

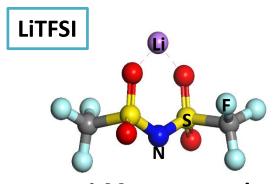


DOL 1,3-dioxolane

DME

1,2-Dimethoxyethane





1 M concentration

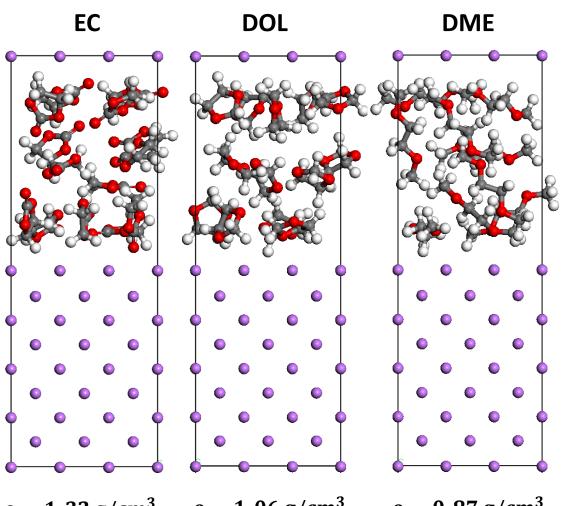
- Optimizations performed using the Vienna ab initio simulation package (VASP)
- Perdew-Burke-Ernzerhof functional (GGA-PBE)
- Cutoff energy: 400 eV
- LiTFSI (G09: B3PW91/6-311++G(p,d))





Methodology

Ab-initio MD simulations at 330 K (~20 ps)



- Ab-initio MD performed using VASP
- GGA-PBE functional
- Cutoff energy: 400 eV
- 2x2x1 k-points Monkhorst—Pack mesh sampling
- Timestep: 1 fs
- NVT ensamble

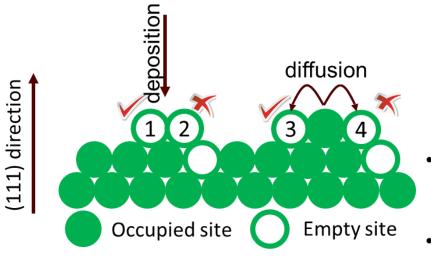
(Pure Solvents)

- $\rho = 1.32 \text{ g/cm}^3$
- $\rho = 1.06 \, \mathrm{g/cm^3}$
- $\rho = 0.87 \text{ g/cm}^3$

Li₂S Growth Model: Deposition + Diffusion

Coarse-Grained Kinetic Monte Carlo Method

- Only consider the insoluble Li₂S molecule deposition on crystal Li₂S (111) surface
- A coarse-grained model is developed to describe the structure of Li₂S (111) film.



 k_0 : reaction rate constant

 N_A : Avogadro constant

V: Volume of electrolyte

S: solid-electrolyte interfacial area

S_a: area per Li₂S unit

C: reactant concentration

Θ: Li₂S solubility

 ν : jump frequency

 E_b : diffusion barrier

 κ : Boltzmann constant

T: temperature

The diffusion process is governed by

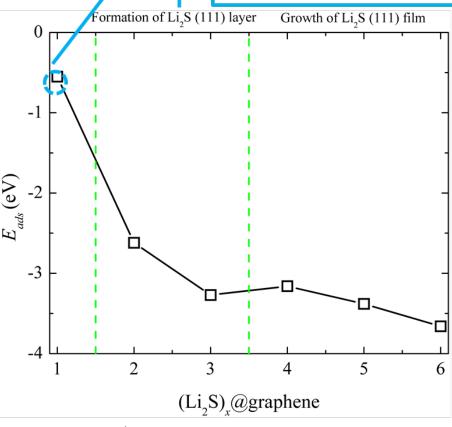
$$K_{dif} = \nu \cdot \exp(-\frac{E_{\rm b}}{\kappa T})$$
.

The deposition process is governed by

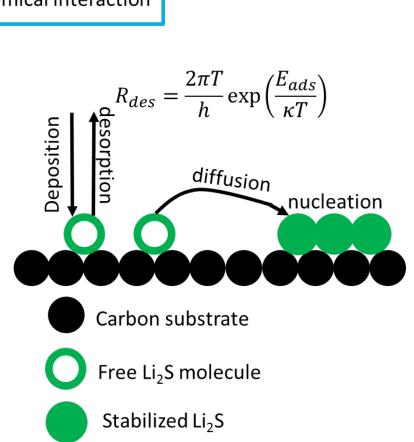
$$K_{dep} = k_0 N_A V \frac{S_a}{S} (C_{Li}^2 + C_{S^{2-}} - \Theta).$$

Li₂S Growth Model: Desorption

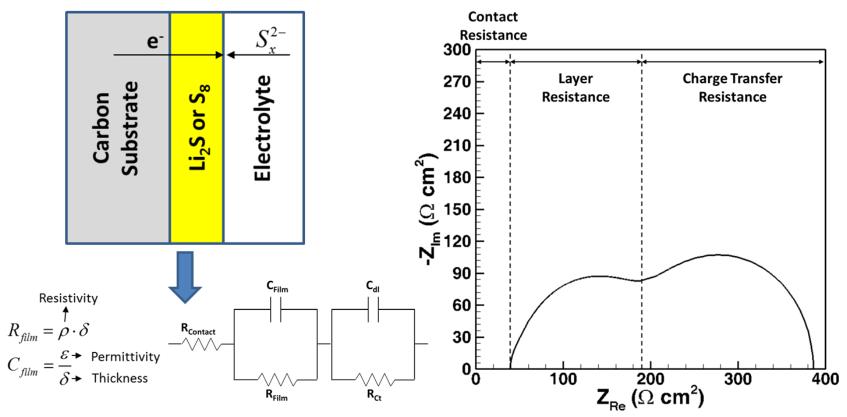
Li₂S desorption should be considered due to the relatively weak chemical interaction



$$E_{ads} = \frac{1}{x} \left(E(G, xLi_2S) - E(G) - xE(Li_2S) \right)$$



Impedance Response of Cathode of Li-S Battery



 $\boldsymbol{R}_{\text{contact}}\text{:}$ Contact Resistance between carbon substrate and thin layer.

 $\mathbf{R}_{\mathsf{Film}}$: Resistance from thin layer.

 $\mathbf{R}_{\mathbf{Ct}}$: Charge transfer resistance from electrochemical reaction.

 C_{Film} : Capacitance from thin layer.

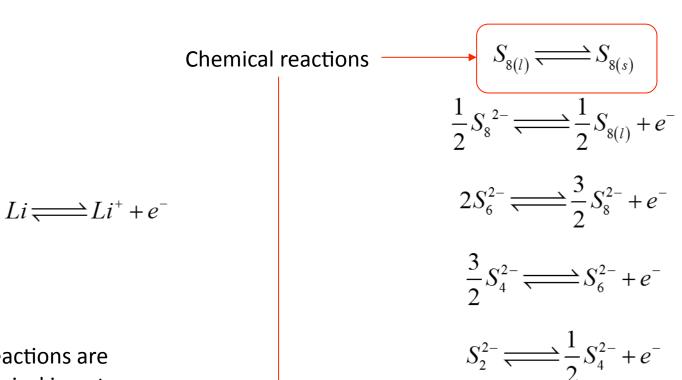
Cd: Capacitance from double layer.

Note: Diffusion resistance is not included and discussed in this model.

Cell Performance Prediction: Electrochemical Reactions

Anodic Reaction

Cathodic Reactions



Other reactions are electrochemical in nature

$$2Li^{+} + S^{2-} \Longrightarrow Li_{2}S \downarrow$$

 $S^{2-} \rightleftharpoons \frac{1}{2}S_2^{2-} + e^{-}$

Cell Performance Prediction: Governing Equations

Balance for species i

$$\frac{\partial}{\partial t} \left(\varepsilon C_i \right) = \nabla \cdot \left(D_i \nabla C_i + z_i \frac{D_i}{RT} F C_i \nabla \phi_e \right) + R_i$$

 C_{i} Concentration

 D_i Diffusivity

Charge conservation

$$\nabla \cdot \left(\sum_{i} z_{i} F \left(D_{i} \nabla C_{i} + z_{i} \frac{D_{i}}{RT} F C_{i} \nabla \phi_{e} \right) \right) = -a \sum_{j} i_{j}$$

 ϕ_e Electric potential in electrolyte

 R_i Species generation rate

Butler-Volmer Equation for reaction *j*

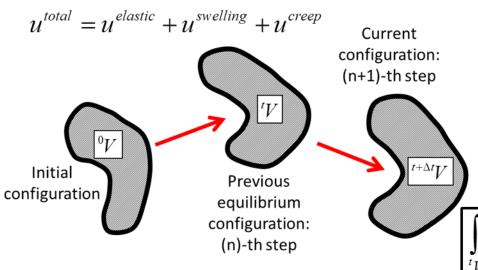
$$M \rightleftharpoons M^{+} + e^{-}$$

$$i_{j} = i_{j}^{0} \left\{ \exp\left(\frac{F}{2RT}\eta_{j}\right) - \left(\frac{C_{M^{+}}}{C_{M^{+}}^{ref}}\right) \exp\left(-\frac{F}{2RT}\eta_{j}\right) \right\}$$

Current generation rate due to electrochemical reaction j

$$\eta_j = \phi_s - \phi_e - U_j$$

Details of Poromechanics: Lattice Spring Method



Nonlinear strain-displacement:

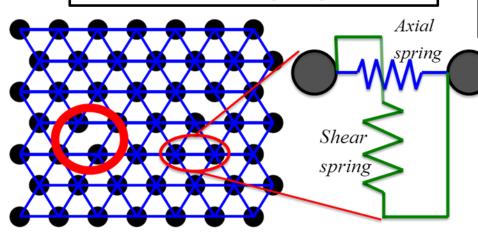
$$\varepsilon_{ij} = \frac{1}{2} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} + \frac{\partial u_k}{\partial x_i} \frac{\partial u_k}{\partial x_j} \right)$$

Governing differential equation:

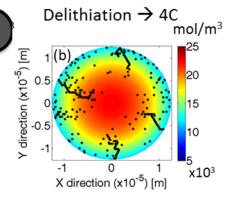
$$\int_{t_{V}} \int_{t}^{t+\Delta t} S_{ij} \delta^{t+\Delta t} \varepsilon_{ij} d^{t}V - \int_{t_{S}} \int_{t}^{t+\Delta t} F_{i} \delta^{t+\Delta t} u_{i} d^{t}V \approx 0$$

 $\varepsilon^{total} \neq \varepsilon^{elastic} + \varepsilon^{swelling} + \varepsilon^{creep}$

Random Lattice Spring Method



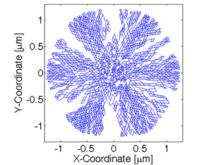
Fracture in Lithium Ion Battery Particles



Internal energy

High capacity anode materials

External energy



Details of Poromechanics: Volume Expansion

$$\frac{d\varepsilon}{dt} = V_{S_{8(s)}} \cdot r_{S_{8(s)}} - V_{Li_2S} \cdot r_{Li_2S} + \Delta \varepsilon_{mech}$$
 Effective volume change due to precipitation induced volume expansion.

• External load is the pressure induced by precipitation:

Bulk modulus of the electrolyte \rightarrow Electrolyte property

Precip $-D_{elec}$ D_{precip} Precipitation induced strain \rightarrow Pore confinement effect

• Precipitation induced strain is given as: $\Delta \varepsilon_{precip} = V_{Li_2S} \cdot \Delta m_{Li_2S} - V_{S_{8(s)}} \cdot \Delta m_{S_{8(s)}}$ $where, \ \Delta m_{Li_2S} = 8\Delta m_{S_{8(s)}}$